

Thermodynamic-Based Model for the Prediction of the Fouling Phenomena in a Wet Phosphoric Acid Process

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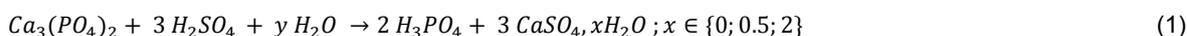
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This paper deals with the development of a thermodynamic-based model for the prediction of fouling phenomena in a wet phosphoric acid process. The developed model is based on mass and heat balances along with equations of Pitzer's thermodynamic model. It involves several unknown parameters that should be identified from experimental data. For this purpose, a database of experimental measurements carried out in this work, and other measurements from the literature are used. The comparison of the available measurements to the predictions generated using the values of the identified parameters shows the high performance of the developed model. Furthermore, the model is used to predict thermodynamic saturation indices of the main minerals that are likely to precipitate during the digestion process, and may cause fouling. A global sensitivity algorithm is finally used to determine the operating parameters that most influence the precipitation of these mineral phases. The results are very consistent with previous works and with the measurements carried out on industrial plants. Moreover, they explain many dysfunctions observed in phosphoric acid production facilities.

1. Introduction

The wet phosphoric acid process is one of the widely used processes to produce industrial phosphoric acid. It consists of a series of reactors where a phosphate-containing mineral (usually apatite) is digested using a concentrated sulfuric acid solution. This process is widely used in industry since it is simple to implement and adaptable to various types of phosphate rock.

During the digestion reaction, sulfuric acid (H_2SO_4) dissociates into H^+ and SO_4^{2-} ions, and at the same time, the phosphate rock releases many phosphorus and calcium-based ions. These ions contribute to the overall digestion reaction (Eq. (1)) (Becker, 1989) which produces liquid phosphoric acid (H_3PO_4) and solid calcium sulfates ($CaSO_4 \cdot xH_2O$).



The reaction shows that H^+ ions (coming from sulfuric acid) attack the phosphorus-based ions to produce liquid phosphoric acid as the main product, whereas the SO_4^{2-} ions react with the calcium-based ions to produce solid calcium sulfates ($CaSO_4 \cdot xH_2O$) as the main by-product. Depending on the operating temperature, the calcium sulfates can be either gypsum ($CaSO_4 \cdot 2H_2O$), bassanite ($CaSO_4 \cdot 0.5H_2O$) or anhydrite ($CaSO_4$).

The digestion reactor outlet stream is separated into liquid and solid products in a filtration unit located downstream of the reactors. The liquid phosphoric acid is then recovered for purification and marketing, while the solid calcium sulfate is stored for later treatment and valorization.

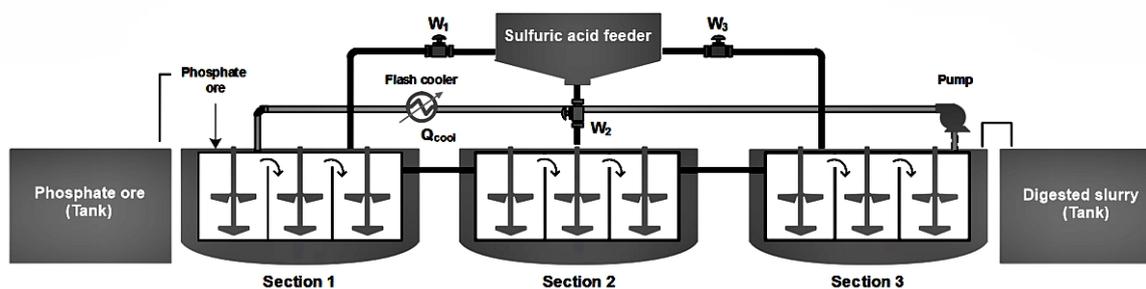


Figure 1: Schematic representation of an industrial phosphate digestion tank with three sections and nine reactors

On an industrial scale (e.g., phosphoric acid plants located in Jorf Lasfar, Morocco), the reaction is carried out in a cylindrical tank made-up of several continuous reactors of the same volume and uniformly distributed (Figure 1). The tank is divided into three sections of three reactors each. Sulfuric acid feed flowrate is spitted into three streams each feeding a section. The phosphate ore is fed into the first reactor of the first section and the product leaves the tank at the last reactor of the last section.

The side reactions, that occur due to impurities coming from the used reagents, are among the problems encountered while using the wet phosphoric acid processes. Indeed, these impurities cause the precipitation of mineral deposits leading to fouling phenomena within the reactors, heat exchangers, pumps, etc. These fouling problems often lead to production shut down for maintenance which is very costly in terms of time, productivity, and safety. The main impurities can be classified into two categories (Becker, 1989; Azaroual et al., 2012). (i) Impurities favoured by the used reagents such as sulfur, fluorine, silica, magnesium, aluminium, organic elements, and heavy metals, and (ii) impurities favoured by the process itself and consist mainly of sodium and potassium coming from the process water.

Based on literature works and history of the exploitation of the wet phosphoric acid processes, it appears that in addition to the production of gypsum ($CaSO_4 \cdot 2H_2O$), bassanite ($CaSO_4 \cdot 0.5H_2O$) and anhydrite ($CaSO_4$) due to the super saturation of the reaction medium by the free sulfates (Becker, 1989), other solid phases can precipitate due to the side reactions caused by the presence of impurities. Indeed, Zmemla et al. (2020), Khamar (2012) and Frazier et al. (1977) proved the existence of brushite ($CaHPO_4 \cdot 2H_2O$) and shukhrovite ($Ca_4SO_4AlSiF_6 \cdot 12H_2O$) by means of scanning electron microscope and X-ray diffraction studies. Furthermore, quantitative X-ray diffraction analysis of quartz are carried out and proved its existence under several crystalline forms including the cristobalite, chalcedony, $SiO_2(a)$ and $SiO_2(am)$. They are produced mainly because of the presence of silica, and their crystalline shape depends on the operating conditions, in particular, temperature and pressure (Zmemla et al., 2020; Khamar, 2012; Waerstad, 1985). Moreover, (Zmemla et al., 2020; Skafi et al., 2019; Frayret et al., 2006; Khamar, 2012) analysed the behaviour of malladrite ($NaSiF_6$) and hieratite ($KSiF_6$) using X-ray diffraction techniques and even through thermodynamic modelling based on water activity measurements. These minerals are produced during the digestion due to the use of untreated process water (usually used for dilution, cooling and other purposes) which brings sodium and potassium components that capture ions of the same polarity and opposite charges such as silica and fluorine ions. Finally, magnesium-based components, e.g. magnesium hexafluorosilicate ($MgSiF_6 \cdot xH_2O$, $x = 0, 6, 7$), are produced during the digestion and may also cause fouling problems. In many works found in literature, these components are studied in order mainly to assess their impact on the filterability of the produced gypsum cake (Rashad et al., 2004; Khamar, 2012).

In this work, we are interested in the simultaneous study of all these competitive fouling phenomena. More specifically, we focus on the development of a thermodynamic model to predict the precipitation of the previously described solid phases and to determine their sensitivity with respect to the operating conditions using a global sensitivity analysis approach.

2. Thermodynamic modelling

A thermodynamic-based model is developed based on mass and heat balance equations, along with the Pitzer thermodynamic model equations (Pitzer, 2018). It is exploited to predict the saturation indices of solid phases used to determine whether a given mineral can precipitate during the digestion process, thus leading to fouling phenomena.

2.1 Saturation index of minerals

The saturation index is used as the main criterion to determine whether the reactive mixture is saturated, under-saturated or super-saturated with respect to a given mineral. The saturation index of a mineral that dissociates or associates as $A_{a_1}^1 A_{a_2}^2 \dots A_{a_n}^n \rightleftharpoons a_1 A^1 + \dots + a_n A^n$ is calculated as:

$$SI = \log\left(\frac{IAP}{K_s}\right) \quad \text{and} \quad IAP = \prod_{i=A^1}^{A^n} (m_i \gamma_i)^{a_i} \quad (2)$$

where IAP is the ion activity product, K_s is the solubility product of the mineral, m_i is the unknown molality of component i and γ_i is its activity coefficient, a_i is the stoichiometric coefficient.

2.2 Thermodynamic-based model

The developed thermodynamic-based model aims to compute the saturation indices of the considered minerals (listed in Table 1) given the operating conditions. As shown in Eq. (2), to compute the saturation indices of these minerals, the molalities m_i and the activity coefficients γ_i of 25 aqueous elements i (Table 1) are needed. They are deduced from a set of equations consisting of 9 material balances (Eqs. (4)), 1 charge balance (Eq. 5), 15 equilibrium constants (presented in Table 2) calculated using Eqs. 6 and 7, and 23 activity coefficients calculated using the Pitzer thermodynamic model (Pitzer, 2018). Finally, it is noteworthy that a heat balance is supported by the model to calculate the operating temperature (Eq. 8).

The resulting nonlinear system of equations involves 50 unknown variables, i.e., 25 molalities and 25 activity coefficients, and 50 equations, which can be solved using a suitable numerical solver.

$$(M)^{tot} = \sum_{i=1}^{NC} \delta_{M,i} m_i \quad M \in \{S, P, F, Si, Ca, Al, Mg, Na, K\} \quad (4)$$

$$\sum_{i=1}^{NC} z_i m_i = 0 \quad (5)$$

$$K_j = \prod_{i=1}^{NR} (m_i \gamma_i)^{\alpha_{i,j}} \quad (6)$$

$$\log(K_j) = \log(K_{j0}) + \frac{\Delta H_j}{R} \left(\frac{1}{T} - \frac{1}{T_0} \right), \quad j = 1, \dots, NR \quad (7)$$

$$Q_H + Q_{AG} + Q_{R+D} = Q_{cool} + Q_{out} \quad (8)$$

where NC and NR are the number of components and reactions respectively, $(M)^{tot}$ is the given total inlet concentration of element M in Eq. (1), m_i is the molality of component i involved in the reactions listed in Table 1, $\delta_{M,i}$ is equal to the number of atoms of element M in component i . For example, the mass balance on (F) develops as: $(F)^{tot} = 6 m_{H_2SiF_6} + m_{F^-} + 6 m_{SiF_6^{2-}} + 4 m_{AlF_4^-} + 6 m_{CaF_2}$. z_i are the electrical charges, γ_i is the activity coefficient of component i . $\alpha_{i,j}$ is the stoichiometric coefficient of component i involved in reaction j . K_{j0} and ΔH_j refer to the equilibrium constant and the enthalpy of the reaction j at $T_0 = 298 K$ respectively, their values are reported in Table 2. Q_H , Q_{AG} , Q_{R+D} , Q_{out} and Q_{cool} are the enthalpy of the inlet products, the agitation heat, the sulfuric acid dilution heat, the enthalpy of the slurry leaving the reactor and the heat to be removed from the process to control the operating temperature respectively.

The Pitzer thermodynamic model (Pitzer, 2018) is used to compute the activity coefficient γ_i as:

$$\ln(\gamma_i) = \frac{z_i^2}{2} f + 2 \sum_j m_j \lambda_{i,j} + z_i^2 \sum_{j,k} m_j m_k \lambda'_{i,j} + 3 \sum_{j,k} m_j m_k \psi_{i,j,k} \quad (9)$$

where i, j, k refer to different components and f is the Debye-Huckel function. $\lambda_{i,j}$, $\lambda'_{i,j}$ and $\psi_{i,j,k}$ are the unknown Pitzer model parameters, they should be determined from the equilibrium measurements carried out in this work and presented in the next section. Furthermore, a suitable estimability analysis method should be used to determine the most estimable parameters from the available data.

Table 1: Mineral phases and their formation-dissolution reactions supported by the developed model

Mineral	Reactions (S \rightleftharpoons Aq)	$\log(K_c)$	References
Fluorapatite	$\text{Ca}_5(\text{PO}_4)_3\text{F} + \text{H}^+ \rightleftharpoons \text{HF} + 3 \text{PO}_4^{3-} + 5 \text{Ca}^{2+}$	-0.910	(Gustafsson, 2011; Ball and Nordstrom, 1991)
Gypsum	$\text{CaSO}_4 \cdot 2\text{H}_2\text{O} \rightleftharpoons \text{Ca}^{2+} + \text{SO}_4^{2-} + 2 \text{H}_2\text{O}$	-4.848	(Gustafsson, 2011)
Bassanite	$\text{CaSO}_4 \cdot 0.5\text{H}_2\text{O} \rightleftharpoons \text{Ca}^{2+} + \text{SO}_4^{2-} + 0.5 \text{H}_2\text{O}$	-3.661	(Gustafsson, 2011)
Anhydrite	$\text{CaSO}_4 \rightleftharpoons \text{Ca}^{2+} + \text{SO}_4^{2-}$	-4.637	(Gustafsson, 2011)
Brushite	$\text{CaHPO}_4 \cdot 0.5\text{H}_2\text{O} \rightleftharpoons \text{Ca}^{2+} + \text{HPO}_4^{2-} + 0.5\text{H}_2\text{O}$	-6.550	(Ball and Nordstrom, 1991)
Shukhrovite	$\text{Ca}_4\text{SO}_4\text{AlSiF}_6 \rightleftharpoons \text{CaSO}_4 + \text{SiF}_6^{2-} + \text{AlF}_4^- + 3\text{CaF}^+$	-19.55	(Zmmla et al., 2020; Fraizer, 1977)
Malladrite	$\text{Na}_2\text{SiF}_6 \rightleftharpoons \text{SiF}_6^{2-} + 2 \text{Na}^+$	-6.475	(Skafi et al., 2019; Azaroual et al. 2012)
Hieratite	$\text{K}_2\text{SiF}_6 \rightleftharpoons \text{SiF}_6^{2-} + 2 \text{K}^+$	-7.039	(Skafi et al., 2019)
Magadiite	$\text{NaSi}_2\text{O}_7 \cdot 3\text{H}_2\text{O} + \text{H}^+ + 9\text{H}_2\text{O} \rightleftharpoons \text{Na}^+ + 7\text{H}_4\text{SiO}_4$	-14.30	(Gustafsson, 2011; Ball and Nordstrom, 1991)
Fluorite	$\text{CaF}_2 \rightleftharpoons \text{Ca}^{2+} + 2 \text{F}^-$	-10.96	(Gustafsson, 2011; Ball and Nordstrom, 1991)
Quartz	$\text{SiO}_2 + 2 \text{H}_2\text{O} \rightleftharpoons \text{H}_4\text{SiO}_4$	-3.018	(Gustafsson, 2011; Ball and Nordstrom, 1991)
MgSiF ₆	$\text{MgSiF}_6 \rightleftharpoons \text{SiF}_6^{2-} + \text{Mg}^{2+}$	-9.960	(Ball and Nordstrom, 1991; Khamar, 2012)
MgSiF ₆ ·6H ₂ O	$\text{MgSiF}_6 \cdot 6\text{H}_2\text{O} \rightleftharpoons \text{SiF}_6^{2-} + \text{Mg}^{2+} + 6 \text{H}_2\text{O}$	-12.96	(Ball and Nordstrom, 1991; Khamar, 2012)
MgSO ₄ ·7H ₂ O	$\text{MgSiF}_6 \cdot 7\text{H}_2\text{O} \rightleftharpoons \text{SiF}_6^{2-} + \text{Mg}^{2+} + 7 \text{H}_2\text{O}$	-14.96	(Ball and Nordstrom, 1991; Khamar, 2012)
CaSiF ₆	$\text{CaSiF}_6 \rightleftharpoons \text{Ca}^{2+} + \text{SiF}_6^{2-}$	-0.519	(Gustafsson, 2011; Ball and Nordstrom, 1991)

Table 2: Aqueous phases supported by the developed model

Equilibria	Reactions	K_{j0}	ΔH_j (J/mol)	References
1	$\text{HSO}_4^- \rightleftharpoons \text{SO}_4^{2-} + \text{H}^+$	0.0103	-1.274 · 10 ⁴	(Gustafsson, 2011; Pitzer, 2018)
2	$\text{H}_3\text{PO}_4 \rightleftharpoons \text{H}_2\text{PO}_4^- + \text{H}^+$	0.0071	-4.271 · 10 ³	(Gustafsson, 2011; Ball and Nordstrom, 1991)
3	$\text{H}_2\text{PO}_4^- \rightleftharpoons \text{HPO}_4^{2-} + \text{H}^+$	6.3 · 10 ⁻⁸	-1.800 · 10 ⁴	(Gustafsson, 2011; Ball and Nordstrom, 1991)
4	$\text{HPO}_4^{2-} \rightleftharpoons \text{PO}_4^{3-} + \text{H}^+$	4.2 · 10 ⁻¹²	-1.500 · 10 ⁴	(Gustafsson, 2011; Ball and Nordstrom, 1991)
5	$\text{H}_3\text{PO}_4 + \text{H}_2\text{PO}_4^- \rightleftharpoons \text{H}_5\text{P}_2\text{O}_8^-$	0.2550	-9.266 · 10 ³	(Khamar, 2012)
6	$\text{HF} \rightleftharpoons \text{F}^- + \text{H}^+$	7.2 · 10 ⁻⁴	-1.329 · 10 ⁴	(Gustafsson, 2011)
7	$\text{H}_2\text{SiF}_6 \rightleftharpoons \text{SiF}_6^{2-} + 2\text{H}^+$	0.3 · 10 ²	-4.799 · 10 ⁴	(Gustafsson, 2011)
8	$\text{H}_4\text{SiO}_4 \rightleftharpoons \text{SiO}_2 + \text{H}_2\text{O}$	3.52 · 10 ⁻⁷	-1.121 · 10 ⁵	(Gustafsson, 2011)
9	$\text{CaF}^+ \rightleftharpoons \text{Ca}^{2+} + \text{F}^-$	1.148 · 10 ⁻⁷	-1.255 · 10 ⁴	(Gustafsson, 2011; Ball and Nordstrom, 1991)
10	$\text{CaSO}_4 \rightleftharpoons \text{Ca}^{2+} + \text{SO}_4^{2-}$	0.6394	-7.200 · 10 ³	(Pitzer, 2018; Shen et al., 2020)
11	$\text{AlSO}_4^+ \rightleftharpoons \text{Al}^{3+} + \text{SO}_4^{2-}$	9.549 · 10 ⁻⁴	-8.368 · 10 ³	(Gustafsson, 2011; Ball and Nordstrom, 1991)
12	$\text{AlF}_4^+ \rightleftharpoons \text{Al}^{3+} + 4\text{F}^-$	9.772 · 10 ⁻⁸	-8.368 · 10 ³	(Gustafsson, 2011; Ball and Nordstrom, 1991)
13	$\text{MgSO}_4 \rightleftharpoons \text{Mg}^{2+} + \text{SO}_4^{2-}$	5.623 · 10 ⁻³	-4.184 · 10 ³	(Gustafsson, 2011; Ball and Nordstrom, 1991)
14	$\text{NaSO}_4^- \rightleftharpoons \text{Na}^+ + \text{SO}_4^{2-}$	0.1995	-4.170 · 10 ³	(Gustafsson, 2011; Ball and Nordstrom, 1991)
15	$\text{KSO}_4^- \rightleftharpoons \text{K}^+ + \text{SO}_4^{2-}$	1.1412	-8.368 · 10 ³	(Gustafsson, 2011; Ball and Nordstrom, 1991)

3. Experimental measurements

Several equilibrium measurements of sulfuric and phosphoric acid solutions are carried out in the laboratory, they consist of pH, conductivity, and density and were used to calculate the molalities of the different ions and molecules (i.e., speciation) involved in the reactive mixtures. To perform these measurements, 98w% sulfuric acid and 65w% phosphoric acid are used. Sulfuric acid measurements are carried out for concentrations ranging from infinite dilution to 4 moles/kgw and temperatures ranging from 298 K to 353 K, whereas, measurements for phosphoric acid are performed for concentrations varying between infinite dilution and 12 moles/kgw, and in the same range of temperature. Several experimental data are also collected from the literature (Shen et al., 2020), they consist of the solubilities of gypsum and anhydrite calcium sulfates in sulfuric acid, carried out at different molality and temperature conditions.

4. Results and discussion

Experimental measurements are used to identify the unknown parameters of the Pitzer thermodynamic model. Beforehand, a parameter estimability analysis was carried out based on our recently developed global estimability algorithm (Bouchkira et al., 2021). This algorithm is used to determine the unknown parameters that are estimable from the available measurements. The most estimable parameters are then identified by minimizing the square-error between the model predictions and the available experimental measurements. Furthermore, the optimization problem was implemented within GAMS environment and a branch-and-reduce algorithm was used to reach the global minimum. The computation time was about three hours using a Dell Precision T7810 Bi-Xeon 12 x Core 64GB Dell Precision workstation. The non-estimable parameters and those for which no experimental measurements are available for their identification are fixed from the literature and from previous works. The values of the interaction parameters are used to compare the predictions of the developed model with experimental measurements, and thus to evaluate the model accuracy. Figures 2 A-C present an example of results, they show the prediction of the speciation of sulfuric and phosphoric acid solutions as well as the solubility of gypsum and anhydrite calcium sulfates at 298 K. The Pearson product-moment correlation coefficient r is also calculated and reported for each case. Its high values demonstrate the very good performance of the developed model.

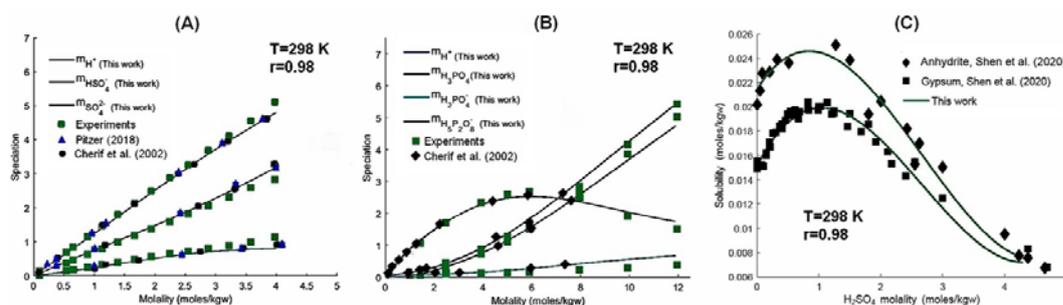


Figure 2: (A) and (B): Sulfuric and Phosphoric acids speciation, (C): gypsum and Anhydrite solubility

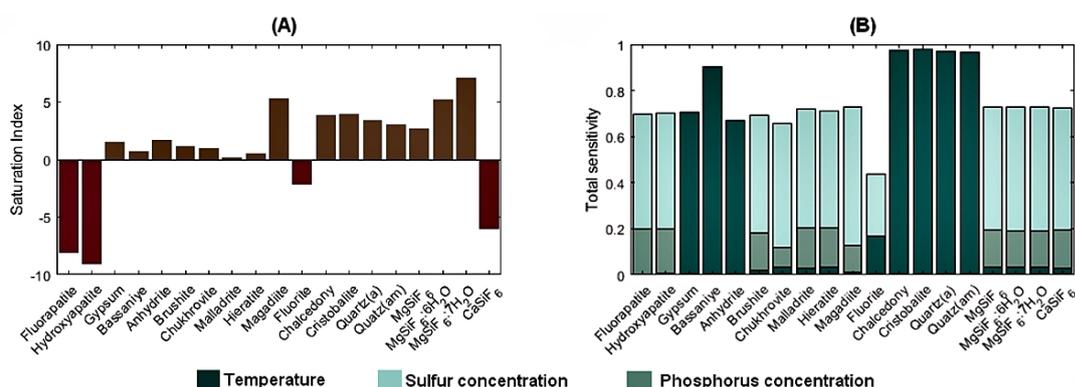


Figure 3: (A): Saturation indices of minerals, (B): Total sensitivity with respect to operating conditions

The saturation indices of minerals in Table 1 are calculated using the developed model and shown in Fig. 3A. Moreover, a global sensitivity analysis algorithm developed by Saltelli (2002) is used to assess the sensitivity of each saturation index with respect to the most important operating conditions (i.e., sulfur and phosphorus concentrations and temperature (Fig. 3.B)). The results show that fluorapatite, hydroxyapatite, fluorite and calcium hexafluorosilicate have negative saturation indices meaning that the thermodynamic conditions of the digestion are favorable for their dissolution and not for their crystallization. This is consistent with the results of Becker (1989) and who studied the dissolution of phosphate-containing minerals in phosphoric acid production processes. The saturation indices of the calcium-based minerals (i.e., gypsum, bassanite and anhydrite) are positive meaning that these minerals are likely to crystallize. Indeed, during the digestion process, the calcium ions released from the phosphate ore tend to capture the free sulfate ions of the same polarity and opposite charges leading to calcium sulfates crystallization. The sensitivity analysis results show that the saturation indices of these minerals are very sensitive to the operating temperature which is very consistent with previous studies (Becker, 1989; Shen et al., 2020). In general, these minerals are considered as principal products of the digestion process and are not involved in the fouling of the process facilities. On the other hand, it is shown that the operating conditions of the digestion are favorable to produce the brushite and shukhrovite as proved by Fraizer (1977) and Zmemla et al., (2020) who studied the existence of these minerals in the gypsum cake obtained in the filtration unit. Meanwhile, Khamar (2012) proved the crystallization of these mineral phases during the cooling of industrial phosphoric acid in storage tanks. Sensitivity analysis shows that the production of these minerals depends mainly on sulfur concentration which is consistent with the results of Becker (1989) and Zmemla et al., (2020). The developed model predicts positive saturation indices for malldrite, hieratite and magadiite, which are mainly produced from the combination of sodium and potassium favoured using untreated process water, and silica and fluorine from the phosphate ore. Azaroual et al. (2012) showed in their work that malladrite presents 68% of the products that cause fouling of the concentration units downstream of the digestion tank, and 96% of the products that cause fouling of the heat exchangers. It is also shown that quartz tends to precipitate in different crystalline forms like chalcedony, cristobalite, $SiO_2(a)$, $SiO_2(am)$. Recently Khamar (2012) and Zmemla et al. (2020) showed their existence by means of X-ray and scanning electron microscopy technologies and their high sensitivity to the operating temperature, moreover, to limit their precipitation, the industrialists advise doping the reaction mixture with aluminum, which favors the fixation of silica and the production of clay and shukhrovite, which are favorable for improving the filterability of the gypsum cake in view of their crystalline form. Finally, the saturation indices of magnesium-containing min-

erals are positive and depend mainly on sulfur concentration. In fact, magnesium is one of the critical impurities involved in several side reactions which cause fouling phenomena and decrease the filterability of the gypsum cake. It is noteworthy that these magnesium-containing minerals are generally characterized by very small sizes, which favours the fouling phenomena (Khamar, 2012) which minimizes the porosity of the gypsum cake and degrades its filterability (Becker, 1989).

5. Conclusions

In this work, a thermodynamic model is developed to enable the prediction of minerals that may precipitate during the digestion of phosphate ore due to side reactions and lead to fouling phenomena. It has been shown that under current production conditions, malladrite, hieratite, magadiite, quartz and magnesium hexafluorosilicate in their different crystalline forms are the most critical minerals that are likely to precipitate and cause fouling phenomena. It is also shown that, limiting the precipitation of some of them requires mainly to operate under an optimal sulfur concentration and temperature which allows to neutralize them or even to limit their production. Moreover, the treatment of the used process water would be an effective solution that should be implemented by the phosphate industries to minimize these fouling problems. Other side reactions that take place during the digestion process were neglected for the sake of simplification; they are mainly due to heavy metals, organic compounds, etc. They should be considered to further improve the accuracy of model.

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